








Microencapsulation of Umami Flavor Enhancer from Indonesian Waters Brown Seaweed

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Abstract

Sargassum aquifolium is a type of brown seaweed that grows in Indonesian waters. The L-glutamic acid in *Sargassum aquifolium* extract can be optimized to be a natural umami flavor enhancer. Spray drying is used for the manufacture of umami flavor enhancing microcapsules, where the core ingredient (extract of *Sargassum aquifolium*) is coated with 10, 20, and 30% (w/v) Maltodextrin (MD). The increase in coating material caused the water content, water activity, and hygroscopicity of the microcapsules to decrease significantly. This is followed by an increase in bulk and tapped density, as well as powder flowability. The particle size distribution is getting smaller and the microcapsule L-glutamic acid levels increased with the addition of the MD concentration. The increase in coating material had a negative impact on the wettability time of the flavor enhancer, the color of the product was slightly degraded but the brightness increased significantly. Meanwhile, the water soluble index and water absorption index for microcapsules did not affect the increase in the coating material. In conclusion, the best umami flavor enhancing microcapsules from *Sargassum aquifolium* seaweed extract were produced by adding 30% MD coating material which was dried by spray drying.

Key-words

Sargassum aquifolium; Umami flavor enhancer; Microencapsulation; Maltodextrin; Spray Drying

Introduction

The utilization of seaweed is not limited as a source of hydrocolloid compounds, it also produces a unique flavor. Components such as free amino acids, 5'-nucleotides, guanosine-5'-monophosphate (GMP), and inosine-5'-monophosphate (IMP) from seaweed synergize with each other which then produces the umami taste. Seaweed's umami compounds have aroused the interest of researchers in recent years¹⁻⁴. The umami compound was discovered by Kikunae Ikeda over a century ago⁵.



The free amino acids (L-glutamate and L-aspartate) in seaweed produce a stronger umami flavor than other compounds ⁶. Free amino acids can be acquired through several methods, such as acid hydrolysis ⁷, enzymatic processes ⁴ to hot extraction of water ¹. The water extraction method is very applicative, environmentally friendly, more economical, with a shorter hydrolysis time ^{8,9}.

Some researchers have hydrolyzed umami compounds from various kinds of brown seaweed ^{1,2,7}, but the umami compound of the brown seaweed of *Sargassum aquifolium* has never been studied. *Sargassum aquifolium* is a brown macroalga that grows in the low intertidal areas, spread across Southeast Asia, and is the most common form of *Sargassum* found in Indonesia ¹⁰. Brown seaweed generally has alginate content, polysaccharides of this hydrocolloid class will form a gel after the hot water extraction process ¹¹, which causes its usage as umami flavoring less than optimal. Furthermore, umami compounds are also easily degraded during processing that involves heat ¹².

The microencapsulation process using the spray drying method is known to be able to increase the thermal stability of umami compounds so that the rate of degradation can be reduced ¹³. Some studies have also confirmed the effectiveness of maltodextrin (MD) as a coating agent in the microencapsulation process of umami compounds ^{8,13,14}. The adding MD ratio is one of the success factors for the microencapsulation of umami compounds ¹⁵. It can significantly increase solubility and reducing the hygroscopic of the products ^{15,16}. However, research related to the microencapsulation of umami compounds from *Sargassum aquifolium* has never been carried out. This study aimed to determine the optimal ratio of MD in the process of microencapsulation of umami flavor enhancer from *Sargassum aquifolium* of Indonesian waters using the spray drying method. This new product could be a potential alternative as a natural umami flavor enhancer



Materials and Methods

Raw Materials

The raw materials used in this study are *Sargassum aquifolium* from the Beach of Garut, West Java, Indonesia and MD with Dextrose Equivalent (DE) 9-13 (Neo-Maldex). *Sargassum aquifolium* is cleaned of impurities such as sand, then dried in a drying cabinet at 50°C for 5 h. The dried *Sargassum aquifolium* was milled and sieved with a 60 mesh sieve. Then seaweed powder stored at low temperature (-20°C) until used.

Extraction of Umami Compounds

Seaweed powder (50 g) soaked in hot water (1000 ml) at 70°C ($\pm 1^\circ\text{C}$) using a magnetic hot plate stirrer. The stirring speed is adjusted to 180 rpm for 30 minutes. The extract was then filtered using Whatman filter paper no. 41, the filtrate was frozen until used^{8,17}.

Microencapsulation of Extract Seaweed

MD was added to the seaweed extract according to treatment (10, 20, and 30%). Each mixture was homogenized separately using a homogenizer at 3000 rpm for 15 minutes. Each emulsion was then dried in a laboratory-scale spray dryer. The drying conditions consist of an inlet air temperature of $120 \pm 2^\circ\text{C}$, the outlet air temperature of $80 \pm 1^\circ\text{C}$, the feed flow rate of 6.0 ml/minute with a pressure of 1.5 bar. The powder obtained is then stored in a metalized vacuum sealer package until used.



Moisture Content and Water Activity

The moisture content of the microcapsule was determined using a moisture analyzer, Shimadzu, MOC63u (Japan). The water activity of the microcapsule was determined using a water activity analyzer, Rotronic, Hygropalm-HP23-Aw-A (Switzerland), at 25°C.

Color Analysis

Color measurement using the Minolta CR-310 Chromameter (Konica Minolta Business Solutions Asia Pte Ltd) calibrated with a standard white ceramic plate ($L^* = 94.95$, $a^* = 0,14$, $b^* = 0,27$) prior to reading. The hue angle, H° and chroma, C° were calculated by using $H^\circ = \tan^{-1} \frac{a^*}{b^*}$ and $C^\circ = (a^2 + b^2)^{1/2}$. The hue angle is used to identify colors (red, yellow, green and blue), whereas chroma distinguishes between bright and dull colors¹⁸.

Hygroscopicity

Each flavor enhancer with known weight was placed in a closed jar separately, the humidity was adjusted using saturated NaCl (Merck) to 75.5%, stored for 7 days with a controlled temperature of 25 °C.

Hygroscopic value (Hg) is expressed in% of water vapor adsorbed by the product which is calculated using the following equation.

$$\text{Hg (\%)} = \frac{\frac{\Delta X}{X+X_i}}{1+\Delta X/X} \times 100$$

Where ΔX = increase in flavor enhancer mass (g), X = flavor enhancer initial mass (g), dan X_i = flavoring water content before exposure to environmental air (% g)¹⁸.



Bulk and Tapped Density

The Bulk Density (BD) value is obtained by pouring an amount of powder flavor enhancer into a 10 mL measuring cup, adjusting it to 0 then weighing it. The sample weight obtained is then divided by the volume of the measuring cup (10 mL) so that the BD value is obtained. The same procedure is also used to obtain the tap bulk density (TBD) value, except when the measuring cup which has been filled with the sample is tapped mechanically until it reaches a constant volume. TBD is calculated using the same formula as BD ^{19,20}.

Compressibility Index and Hausner Ratio

Compressibility index or Carr index (CI) and Hausner Ratio (HI) were used to measure the flow power of powder samples. Both are obtained from the density of the mass and tapped density of the flavor enhancer using the following equation: $CI (\%) = (TBD - BD)/TBD \times 100$, and $HI = TBD/BD$ ²¹.

Wettability

Wettability was acquired after some flavor enhancer samples (10 g) were poured into 100 ml of distilled water that was already available in a 250 ml chemical glass. The time it takes for the sample to first touch the water surface until it is completely wet is a wettability value ²².

Water Solubility Index (WSI) and Water Absorption Index (WAI)

The water solubility index (WSI) was obtained by careful weighing of the flavor-enhancing powder 1.0 g, mixed in 30 ml of water, and incubated for 30 minutes in a water bath at 30 ° C. The mixture was then



centrifuged for 15 minutes at 3000 rpm. The supernatant obtained was collected into a known weight of petri dishes, while the residue was weighed after drying for 8 hours in an oven at 105 ° C and expressed as the WSI value that had been accumulated with the initial sample weight (1.0 g). The water absorption index (WAI) is calculated based on the mass of solids remaining in the supernatant divided by the initial sample weight (1.0 g) ²³.

Particle Size Analysis

Particle size distribution was measured using a particle size analyzer LLPA-C10 (Labtron), with the principle of laser light scattering with a measurement range for dry disperse 0.01 - 2000 µm.

L-glutamic acid

L-glutamic content measured by the increase in absorbance at 492 nm using the L-glutamic acid assay kit from megazyme.

Results and Discussion

Moisture Content and Water Activity

The umami flavor enhancer from seaweed has low moisture content and aw (Table 1), indicating good efficiency of the drying process and product stability, microbial growth will not be optimal so that the product shelf life will be long ²⁰. This result is following other studies, which used MD as a coating material in the encapsulation process for umami compounds ⁸, while Fazaili *et al.*, ²⁴ also observed a decrease in water content with an increase in the concentration of the carrier material which is dried with various concentrations of MD. The use of MD in the flavor-enhancing microencapsulation process



resulted in moisture content within the desired range (3.10 - 3.63%). The water content of microcapsules coated with MD by spray drying generally ranges from 2.11 to 4.66%^{25,26}.

Similar to water content, the aw value of the flavor enhancer also decreases with the addition of MD as a coating material, in line with research conducted by Nambiar *et al.*,²⁷. However, excessive concentrations of MD will cause the product to stick to the nozzle and block the hot steam. The increase in MD up to 30% caused the aw value of the product to decrease from 0.25 to 0.23, which was previously confirmed by Cao *et al.*,²⁸. Aw values below 0.60 for powder products are good, able to suppress microbial growth, while aw values of 0.2 - 0.4 are considered the most optimal because they are stable against adverse reactions such as oxidation, browning, hydrolytic, to enzymatic^{29,30}.

Tabel 1. Water content, Aw, hygrosopicity, water soluble index and water absorption index of microcapsules

Concentration of MD	Water Content (%)	Aw	Higrosopicity (%)	WSI (%)	WAI (%)
10%	3.63 ± 0.11 ^c	0.26 ± 0.02 ^c	20.56 ± 0.61 ^c	93.18 ± 0.43 ^a	0.03 ± 0.01 ^a
20%	3.23 ± 0.05 ^b	0.23 ± 0.01 ^b	17.88 ± 0.38 ^b	93.46 ± 0.50 ^a	0.05 ± 0.01 ^a
30%	3.10 ± 0.03 ^a	0.21 ± 0.01 ^a	15.47 ± 0.42 ^a	94.49 ± 0.18 ^a	0.06 ± 0.01 ^a

Note: The data are representations of the mean values ± standard deviation. Different superscripts in the same column showed statistically significant differences (p <0.05).

Hygrosopicity

Hygrosopicity in the food sector is closely related to the porosity and amorphous sugar content of the product. The powder produced by spray-drying tends to form amorphous solids, the process of evaporation of water material takes place quickly so that the product is more hygrosopic³¹. The umami flavor enhancer has a fairly good hygrosopicity value with a value range of 15.47 - 20.56%, higher than



that reported by Gagnetten *et al.*,³². Apart from being hygroscopic, spray drying products have a porous surface structure and a low glass transition temperature (T_g). Improper handling after drying, allows the product moisture content to increase. The addition of coatings is very effective in correcting these deficiencies^{23,33}. MD has anti-hygroscopic properties which can change the balance of hydrophilic/hydrophobic particles, which results in lower water absorption¹⁵.

Water Solubility Index and Water Absorption Index

The ideal powder product has a high WSI value. There can be no significant differences in the sample WSI. However, the powder WSI value was higher when the MD concentration increased. In general, the solubility of the product was very good (93.18 - 94.49%), the presence of MD increased the solubility of atomized samples. This is due to the very high hydroxyl (OH) group in the MD molecule. MD also produces a more porous powder microstructure, so that the powder will more easily dissolve in water^{18,34}. The umami compounds in the extract are also hydrophilic. Umami compounds will interact with taste receptors when they meet saliva, one of the unique and important characteristics of food flavor enhancers⁸.

Unlike the case with WSI, WAI is a solid that remains after the centrifugation process. The concentration of WAI is generally very small and was confirmed in this study. Taste enhancers had WAI values in the range of 0.03 - 0.06%, there was no statistically significant difference. The same result was also reported by Vidović *et al.*,²³, the low value of WAI was influenced by the hydrophilic group of the particles that bind water molecules which then form a gel. The values of WSI and WAI are the determining factors for the quality of powders used in the food industry. The industry prefers powder products with high WSI values and low WAI, powders with poor solubility can cause high economic losses for companies³⁵.



Wettability and Particle Size

Apart from high solubility, flavor enhancers should ideally also have a fast wettability, do not float and sink completely. The average wettability time of the seaweed flavor enhancer ranged from 427 to 689 s, faster than the wettability of the sumac extract microcapsules (1239 - 3263 s) reported by Caliskan & Dirim²⁹, but longer than the wettability of the spray-dried blackberry microcapsules with the same coating material³⁶. Although it has high solubility and porous particle structure^{37,38}, the main component of MD preparation is starch so it requires a longer wettability time³⁹. There are several ways to speed up the wettability time, such as the addition of inulin in the coating material formulation which has been confirmed to be able to significantly shorten the wettability time of the spray drying powder³⁵. Several other aspects such as a decrease in the drying temperature (inlet or outlet) and the concentration of the coating material will cause a faster wettability time, due to the size and structure of the resulting particles.

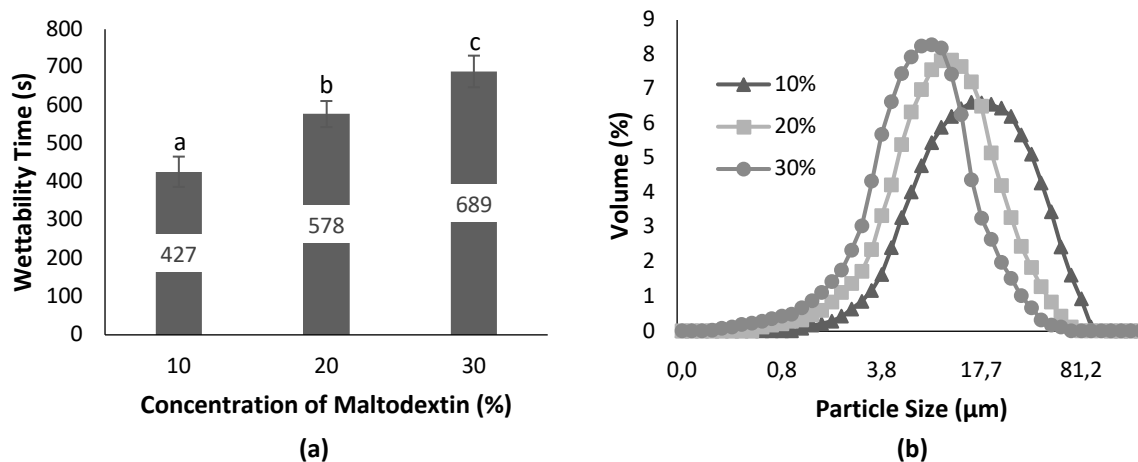


Figure 1: (a) Wettability time, and (b) Microcapsule Particle Size Distribution.



The particle size of the umami flavor enhancers of *Sargassum aquifolium* ranges from 0.19 - 94.57 μm , smaller than that reported by Mayasari *et al.*,¹⁶ (43-14 - 101.71 μm). The particle size distribution of each coating concentration was observed, flavor enhancers with MD 30% produced the smallest particle size distribution (0.19 - 59,371 μm) with a dominant size of 5.21 - 11.17 μm (47.51%), and a peak size of 8.23 μm , flavor enhancers with MD 20% produced particles with a size distribution of 0.62 - 69.60 μm , dominant size 8.23 - 7.21 (38.06% 0, with a peak size of 11.17 μm , while flavor enhancers with 10% MD had the largest particle size distribution (1.13 - 94.57 μm) with the size dominant 11.17 - 27.90 μm (45.05%), and peak particle size at 15.16 μm . In general, the umami flavor enhancer from *Sargassum aquifolium* has a fine powder with a small particle size. Medina-Torres *et al.*,⁴⁰ reported that the results of microcapsules by spray drying with MD coating material have a very small size distribution (10.00 to 40.00 μm), with a rough, hollow, irregular surface morphology with structural cracks on the surface. The high drying temperature will result in smaller particles with finer and more rounded morphology^{16,34}.

Colour Parameters

The color attribute is one of the sensory attractions that need attention. Ideally, the flavor enhancer should be a bright color so that it doesn't affect the final color of the product when added. The seaweed extract used tends to be brown with details $L^* = 58.31$; $a^* = 6.29$ and $b^* = 20.16$, while the MD used is bright white ($L^* = 97.83$; $a^* = 0.21$ and $b^* = 1.94$). The L^* value of flavor enhancement significantly increased (76.76 to 81.49), resulting from the dominant white color of MD⁴¹. a^* (4.32 to 3.16) and b^* (16.35 to 14.29) values decreased as the coating agent concentration increased. MD produced good retention of flavor-enhancing pigments. This result was in line with the color change of the tea water extract microcapsules coated MD with spray drying reported by Nadeem *et al.*⁴². The hue angle is related to the color produced, the value 0° representing red and 90° representing yellow. With increasing MD



concentration, the color change towards yellow is getting bigger, where the hue angle from 75.18 to 77.52, while the chroma value decreases (16.91 to 14.64), it is possible because high temperatures cause the color pigment to degrade slightly²⁷. Caparino *et al.*,¹⁸ also explained that spray drying resulted in very small particle size so that the resulting mango powder was brighter. The increase in brightness will cause a decrease in color sharpness (Chroma) in addition to the effect of white MD.

Table 2. Discoloration of microcapsules with various concentrations of coating ingredients

Concentration of MD	L^*	a^*	b^*	C°	Hue Angle
10%	76.76 ± 0.91^a	4.32 ± 0.12^c	16.35 ± 0.22^c	16.91 ± 0.23^c	75.18 ± 0.37^a
20%	79.60 ± 0.97^b	3.46 ± 0.09^b	15.42 ± 0.15^b	15.80 ± 0.16^b	77.35 ± 0.24^b
30%	81.49 ± 0.21^c	3.16 ± 0.33^a	14.29 ± 0.56^a	14.64 ± 0.56^a	77.52 ± 1.33^c

Note: The data are representations of the mean values \pm standard deviation. Different superscripts in the same column showed statistically significant differences ($p < 0.05$).

Bulk and Tapped Density, Carr Index and Husner Ratio

Powder flowability can be determined by the value of bulk and tapped density, Carr Index, and Hausner Ratio. The bulk and tapped density values for the umami flavor enhancer can be seen in Table 3. The bulk density of seaweed flavor enhancer powder was found to be greater in microcapsules coated with 30% MD (0.46 g / ml), as well as the tapped density of powder at the same concentration (0.54 g / ml). MD particles that are bigger than the core particles will cause the density of the powder produced to increase with the addition of MD. Besides, powders with lower water content are also known to have a greater density^{42,43}. This is in line with what Singh *et al.*,⁴⁴ reported, an increase in the concentration of MD up to 3x which was dried by spray drying would cause the tapped density of powder to increase from 0.38 - 0.44 g / ml.



The increase in coating material concentration also has an impact on decreasing the volume of particles, which is caused by decreased air formation in the structure, so that the bulk and tapped density increases¹⁹. In contrast to coating materials, an increase in intake air temperature tends to result in a lower bulk particle density¹⁶. An increase in inlet temperature followed by a decrease in the feed flow rate causes the outer dry layer of the droplet surface to form rapidly, the outside will form a moisture-proof film while the inside forms a hollow structure²⁰. When the hollow structure decreases, the particle volume decreases, which affects the cohesiveness of the particles. The cohesiveness of the structure is an important indicator of powder flow properties, expressed by CI and HR values.

Table 3. Bulk and tapped density, Carr Index, and Hausner Ratio of microcapsules

Concentration of MD	Bulk Density (g/ml)	Tab Bulk Density (g/ml)	Carr Index (%)	Hausner Ratio
10%	0.31 ± 0.02 ^a	0.38 ± 0.03 ^a	18.60 ± 0.93 ^c	1.23 ± 0.01 ^c
20%	0.37 ± 0.02 ^b	0.45 ± 0.02 ^b	17.41 ± 0.60 ^b	1.21 ± 0.01 ^b
30%	0.46 ± 0.02 ^c	0.54 ± 0.03 ^c	14.17 ± 0.45 ^a	1.17 ± 0.01 ^a

Note: The data are representations of the mean values ± standard deviation. Different superscripts in the same column showed statistically significant differences ($p < 0.05$).

Deshmukh *et al.*,⁴⁵ stated that spray drying generally results in a narrower particle size distribution with excellent flow properties. High CI and HR values indicate higher particle cohesiveness, and poor flowability²⁰. According to Lebrun *et al.*,²¹ a good powder has the criteria for the CI value of ≤ 15 and the Hausner Ratio value of ≤ 1.18 . The flowability of the flavor-enhancing powder with MD 10% and 20% was still acceptable, the best flowability was produced after the addition of 30% coating material with CI values of 14.17 (good) and HR 1.17 (good). These results are consistent with the findings reported by Cao *et al.*,²⁸. Products with higher HR tend to be cohesive, characterized by a higher moisture content³⁹.



Also, particle size, hardness, surface shape, elasticity to interstitial air determine the cohesiveness of the powder which determines the product flowability ¹⁵.

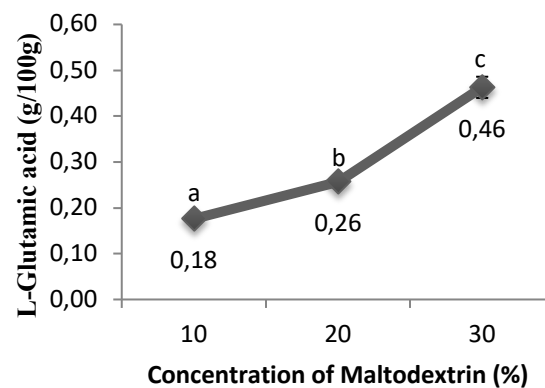


Figure 2. L-Glutamic Acid Content of Umami Flavor Enhancing Microcapsules

Glutamic Acid Content

The presence of glutamic acid is the most important factor in flavor enhancers because it determines the taste of umami produced. MD as a coating material is quite effective in protecting umami compounds from *Sargassum aquifolium* extract, where microcapsules with a 30% MD concentration have the highest L-glutamic acid (0.46 g / 100g), while the lowest is at 10% MD concentration. This indicates that MD has a chemical structure suitable for the core material, strengthened by previous research ¹⁶. The chemical structure of the wall material that is not suitable will cause the coating of the core material to be not optimal so that a lot of it is wasted. The smaller the particle size, the more likely it will form a whole spherical structure like a ball which is known to be able to maintain the flavor-enhancing compounds optimally ⁴⁶. MD is also known to be able to significantly increase the thermal stability of flavor-enhancing



microcapsules and improve the controlled release of microcapsules for up to 60 minutes in boiling water

12,13.

Conclusion

Based on the analysis of physical and chemical characteristics, the best umami flavor enhancing microcapsules from the *Sargassum aquifolium* seaweed extract from spray drying were produced by adding 30% MD. The umami flavor enhancing microcapsules have low water content (3.10%), aw (0.21), and Hg (15.47%), which are good for product shelf life because they are able to withstand the rate of damage both biologically, chemically and physically. Although the product wettability time is relatively long (689 s), the microcapsules have excellent solubility quality (WSI 94.49% and WAI 0.06%) and are favored by the industrial world. The powder is slightly yellowish-brown in color with good brightness ($L^* 81.49$, $a^* 3.16$, $b^* 14.29$, $C^\circ 14.64$, $H^\circ 77.52$). The product flowability and cohesiveness were good, as indicated by the bulk and tapped density values of 0.46 g / ml and 0.54 g / ml, then CI 14.17 and HR 1.17. The powder particle size ranged from 0.19 to 59.37 μm with L-glutamic acid levels reaching 0.46 g / 100 g.

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Conflict of Interest

The authors declare no conflict of interest.



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ACCEPTANCE LETTER

M

Managing Editor <info@foodandnutritionjournal.org>

to me ▾

Dear Dr Diode,

Thanks for your email. We are glad to inform you that your manuscript has been accepted by our editorial board for the next issue. We will soon send you the acceptance cum bill for the same.

Best Regards

Sobiya Sultan

Editorial Assistant

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Is the statistical analysis sound and justified? (Does it require expert statistical review?) Yes No

Other Comments?

Comments per section of manuscript:

Abstract	Change “Meanwhile, the water soluble index” to “ <u>Meanwhile, the water soluble index and water absorption index for microcapsules did not increase the coating material's increase.</u> ”
Introduction	Change “Free amino acids can be acquired through.....” to “Free amino acids can be acquired through several methods, such as acid hydrolysis ⁷ , enzymatic processes ⁴ , and hot water extraction ¹ . The water extraction method is very applicative, environmentally friendly, and economical, with a shorter hydrolysis time of ^{8,9} .”
Methodology	What is megazyme???
Results and Discussion	Change aw (Moisture Content and Water Activity section) and Aw (Table1) to a _w
References (Appropriateness)	

Rating (1 to 5) 5: Excellent, 1: Poor

Originality	5
Depth of research	5
Technical quality	5

Recommendation:

- Reject unconditionally
- Reject in current form, but allow resubmission after revision as per my accompanying comments
- Accept conditionally, subject to minor revision, according to my accompanying comments**
- Accept unconditionally



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Medium

Does the paper compliant with the aims and scope of the journal it is submitted to? X Yes No

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Does the paper include animal or human study? If yes, was ethical committee approval details provided in the paper? Yes X No Not Applicable

Is this a human intervention study? Was consent taken before the study? Yes No X Not Applicable

Is the statistical analysis sound and justified? (Does it require expert statistical review?) Yes X No

Other Comments?

Comments per section of manuscript:

Abstract	It's OK
Introduction	It's OK
Methodology	This section should be explained in a better way. Also the model of used infrastructures should be included, for example Spry-dyer. In addition, it should be explained the methodology used to determine the L-glutamic acid content and the spectrophometer model used to measure the absorbance at 492 nm.
Results and Discussion	In the first step, a chromatographic analysis of the Seaweed powder extract should be carried out and included in the study. In addition, the morphology of the obtained capsules should be analyzed by SEM. The results obtained with MD% higher than 30% should be presented in the paper to analyze the effect. I suggest the authors to analyze also the addition Cyclodextrins (CDs) in combination with MD for the extract encapsulation. In general this cyclic oligosaccharides increased the stability of different extract types. Tables should be presented a bit more elaborately way. Figure 1a, X axis legend should be replaced by "MD concentration (%)". Table 2 legend should be "CIELAB colour parameters of microcapsules". Table 3, TaD should be replaced by "Tapped". Figure 2: a, b and c should be eliminated from the figure because they are not explained in the legend and do not contribute with additional information. Figure 2, X axis legend should be replaced by "MD concentration (%)".
References (Appropriateness)	OK

Rating (1 to 5) 5: Excellent, 1: Poor

Originality	3
Depth of research	3
Technical quality	4

Recommendation:

Reject unconditionally

Reject in current form, but allow resubmission after revision as per my accompanying comments

Accept conditionally, subject to minor revision, according to my accompanying comments

Author's Response to Reviewer's Comments

Reviewer number 1

Paper title: **Microencapsulation of Umami Flavor Enhancer from Indonesian Waters Brown Seaweed**

Title	Reviewer's Comments	Author's Response
Abstract	Change "Meanwhile, the water soluble index" to " <u>Meanwhile, the water soluble index and water absorption index for microcapsules did not increase the coating material's increase.</u> "	The text has been revised and adapted to reviewer input.
Keywords	-	-
Introduction	Change "Free amino acids can be acquired through....." to "Free amino acids can be acquired through several methods, such as acid hydrolysis ⁷ , enzymatic processes ⁴ , and hot water extraction ¹ . The water extraction method is very applicative, environmentally friendly, and economical, with a shorter hydrolysis time of ^{8,9} ."	The text has been revised and adapted to reviewer input.
Methodology	What is megazyme???	Megazyme is an L-Glutamic Acid test kit with enzymatic principle. A very reliable, fast and accurate method for the measurement and analysis of



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		L-glutamate in foodstuffs. The latest research using the megazyme kit in the analysis of glutamic acid content entitled "Free Amino Acid and Volatile Compound Profiles of Jeotgal Alternatives and Its Application to Kimchi" can be accessed through https://www.mdpi.com/2304-8158/10/2/423/htm
Results and Discussion	Change aw (Moisture Content and Water Activity section) and Aw (Table1) to a_w	The text has been revised and adapted to reviewer input.
Conclusion	-	-
References (Appropriateness)	-	-

Author's Response to Reviewer's Comments

Reviewer number 2

Paper title: **Microencapsulation of Umami Flavor Enhancer from Indonesian Waters Brown Seaweed**






Title	Reviewer's Comments	Author's Response
Abstract	It's OK	-
Keywords	-	-
Introduction	It's OK	-
Methodology	This section should be explained in a better way. Also the model of used infrastructures should be included, for example Spray-dryer. In addition, it should be explained the methodology used to determine the L-glutamic acid content and the spectrophotometer model used to measure the absorbance at 492 nm.	We've improved the research method, we have included all the infrastructure models used. Methodology used to determine the L-glutamic acid content and the spectrophotometer model used to measure the absorbance at 492 nm, have been well added.
Results and Discussion	In the first step, a chromatographic analysis of the Seaweed powder extract should be carried out and included in the study. In addition, the morphology of the obtained capsules should be analyzed by SEM. The results obtained with MD% higher than 30%	We've done to do the analysis, according to the reviewer's direction, namely the analysis of seaweed powder extract (figure 1) and capsule morphology using SEM (figure 3). The reviewer's input was very good (addition Cyclodextrins (CDs) in



	<p>should be presented in the paper to analyzed the effect.</p> <p>I suggest the authors to analyze also the addition Cyclodextrins (CDs) in combination with MD for the extract encapsulation. In general this cyclic oligosaccharides increased the stability of different extract types. Tables should be presented a bit more elaborately way.</p> <p>Figure 1a, X axis legend should be replaced by “MD concentration (%)”.</p> <p>Table 2 legend should be “CIELAB colour parameters of microcapsules”.</p> <p>Table 3, TaD should be replaced by “Tapped”.</p> <p>Figure 2:a, b and c should be eliminated from the figure because they are not explained in the legend and do not contributed with additional information.</p> <p>Figure 2, X axis legend should be replaced by “MD concentration (%)”.</p>	<p>combination with MD for the extract encapsulation). We’ve to contact suppliers of CDs abroad, considering that in our country it’s not yet available. However, the delivery process can take up to 3-4 months, plus a quarantine period in Indonesian customs department. The process will take longer considering the rules during the COVID-19 pandemic in Indonesia. The reviewer’s input give us an idea, to do further research after this article was published.</p> <p>We’ve adjusted each table and figure according to the reviewer’s input properly.</p>
Conclusion	-	-
References (Appropriateness)	OK	-



Microencapsulation of Umami Flavor Enhancer from Indonesian Waters Brown Seaweed

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Abstract

Sargassum aquifolium is a type of brown seaweed that grows in Indonesian waters. The L-glutamic acid in *Sargassum aquifolium* extract can be optimized to be a natural umami flavor enhancer. Spray drying is used for the manufacture of umami flavor enhancing microcapsules, where the core ingredient (extract of *Sargassum aquifolium*) is coated with 10, 20, and 30 % (w/v) Maltodextrin (MD). The increase in coating material caused the water content, water activity, and hygroscopicity of the microcapsules to decrease significantly. This is followed by an increase in bulk and tapped density, as well as powder flowability. The particle size distribution is getting smaller, with smooth surface morphology and uniform shape, and the microcapsule L-glutamic acid levels increased with the addition of the MD concentration. The increase in coating material had a negative impact on the wettability time of the flavor enhancer, the color of the product was slightly degraded but the brightness increased significantly. Meanwhile, the water soluble index and water absorption index for microcapsules did not increase the coating material's increase. In conclusion, the best umami flavor enhancing microcapsules from *Sargassum aquifolium* seaweed extract was produced by adding 30 % MD coating material which was dried by spray drying.

Key-words

Sargassum aquifolium; Umami flavor enhancer; Microencapsulation; Maltodextrin; Spray Drying

Introduction

The utilization of seaweed is not limited to a source of hydrocolloid compounds, it also produces a unique flavor. Components such as free amino acids, 5'-nucleotides, guanosine-5'-monophosphate (GMP), and inosine-5'-monophosphate (IMP) from seaweed synergize with each other which then produces the umami taste. Seaweed's umami compounds have aroused the interest of researchers in recent years¹⁻⁴. The umami compound was discovered by Kikunae Ikeda over a century ago⁵. The free amino acids (L-glutamate and L-aspartate) in seaweed produce a stronger umami flavor than other compounds⁶. Several methods can acquire free amino acids, such as acid hydrolysis⁷,



enzymatic processes ⁴, and hot water extraction ¹. The water extraction method is very applicative, environmentally friendly, and economical, with a shorter hydrolysis time of ^{8,9}.

Some researchers have hydrolyzed umami compounds from various kinds of brown seaweed ^{1,2,7}, but the umami compound of the brown seaweed of *Sargassum aquifolium* has never been studied. *Sargassum aquifolium* is a brown macroalga that grows in the low intertidal areas, spread across Southeast Asia, and is the most common form of *Sargassum* found in Indonesia ¹⁰. Brown seaweed generally has alginate content, polysaccharides of this hydrocolloid class will form a gel after the hot water extraction process ¹¹, which causes its usage as umami flavoring less than optimal. Furthermore, umami compounds are also easily degraded during processing that involves heat ¹².

The spray drying method of microencapsulation has been shown to improve the heat stability of umami compounds, hence reducing the rate of degradation ¹³. Maltodextrin (MD) has also been shown to be useful as a coating material in the microencapsulation of umami compounds in several studies ^{8,13,14}. One of the key criteria for the microencapsulation of umami chemicals is the addition of an MD ratio of ¹⁵. It can considerably improve product solubility while lowering hygroscopicity ^{15,16}. However, there has never been any research on the microencapsulation of umami chemicals from *Sargassum aquifolium*. This study aimed to determine the optimal ratio of MD in the process of microencapsulation of umami flavor enhancer from *Sargassum aquifolium* of Indonesian waters using the spray drying method. As a natural umami taste enhancer, this new product might be a viable option.



Materials and Methods

Raw Materials

The raw materials used in this study are Sargassum aquifolium from the Beach of Garut, West Java, Indonesia, and MD with Dextrose Equivalent (DE) 9-13 (Neo-Maldex). Sargassum aquifolium is cleaned of impurities such as sand, then dried in a drying cabinet (OVG-12, Agrowindo, Indonesia) at 50 °C for 5 h. The dried Sargassum aquifolium was milled (disc mill model AGC-15, Agrowindo, Indonesia) and sieved with a 60 mesh sieve. Then seaweed powder is stored at low temperature (-20 °C) until used.

Extraction of Umami Compounds

Seaweed powder (50 g) soaked in hot water (1000 mL) at 70 °C (± 1 °C) using a magnetic hot plate stirrer (Ika Magnetic Stirrers C-MAG HS7). The stirring speed is adjusted to 180 rpm for 30 minutes. The extract was then filtered using Whatman filter paper no. 41, the filtrate was frozen until used^{8,17}.

Microencapsulation of Extract Seaweed

MD was added to the seaweed extract according to treatment (10, 20, and 30 % w/v). Each mixture was homogenized separately using a homogenizer (Daihan HG-15D, Daihan Scientific Co., Ltd) at 3000 rpm for 15 minutes. Each emulsion was then dried in a BUCHI Mini Spray Dryer B-190. The drying conditions consist of an inlet air temperature of 120 ± 2 °C, an outlet air temperature of 80 ± 1 °C, and a feed flow rate of 6.0 mL/minute with a pressure of 1.5 bar. The powder obtained is then stored in a metalized vacuum sealer package until used.



L-glutamic acid

L-glutamic content was measured using the L-glutamic acid assay kit from Megazyme (K-Glut, Ireland), which is measured by the increase in absorbance at 492 nm using a spectrophotometer (Shimadzu UV Vis-1601). 0.1 mL of the diluted flavor enhancer sample with 2.0 mL of distilled water, 0.5 mL of solution 1 (35 mL of buffer pH 8.6 plus 0.02% sodium azide w/v), 0.2 mL of solution 2 (nicotinamide-adenine dinucleotide/NAD⁺ plus idonitrotetrazolium chloride/INT), and 0.05 mL of suspension 3 (diaphorase). Let stand for 2 minutes, then read the absorbance at 492 nm (A1). Then add 0.05 mL of solution 4 (glutamate dehydrogenase/GDH), and let stand. Read the absorbances of the solutions at the end of the reaction (approx. 8-10 min) (A2). $\Delta A_{L\text{-glutamic acid}}$ is obtained after the final values A2-A1.

The concentration of L-glutamic acid can be calculated as follow:

$$c = \frac{V \times MW}{\epsilon \times d \times v} \times \Delta A_{L\text{-glutamic acid}} \text{ (g/L)}$$

Where:

- V = final volume (2.90 mL)
- MV = molecular weight of L-glutamic acid (147.13 g/mol)
- ϵ = extinction coefficient of INT-formazan at 492 nm
= 19900 ($1 \times \text{mol}^{-1} \times \text{cm}^{-1}$)
- d = light path (1.0 cm)
- v = sample volume (0.1 mL)

Moisture Content and Water Activity (a_w)

The moisture content of the microcapsule was determined using a moisture analyzer, Shimadzu, MOC63u (Japan). The a_w of the microcapsule was determined using a water activity analyzer, Rotronic, Hygropalm-HP23-Aw-A (Switzerland), at 25 °C.



Color Analysis

Color measurement using the Minolta CR-310 Chromameter (Konica Minolta Business Solutions Asia Pte Ltd) calibrated with a standard white ceramic plate ($L^* = 94.95$; $a^* = 0.14$; $b^* = 0.27$) prior to reading. The hue angle, H° and chroma, C° were calculated by using $H^\circ = \tan^{-1} \frac{a^*}{b^*}$ and $C^\circ = (a^2 + b^2)^{1/2}$. The hue angle is used to identify colors (red, yellow, green, and blue), whereas chroma distinguishes between bright and dull colors ¹⁸.

Hygroscopicity

Each flavor enhancer with known weight was placed in a closed jar separately, the humidity was adjusted using saturated NaCl (Merck) to 75.5 %, stored for 7 days with a controlled temperature of 25 °C. Hygroscopic value (Hg) is expressed in% of water vapor adsorbed by the product which is calculated using the following equation.

$$\text{Hg (\%)} = \frac{\frac{\Delta X}{X+X_i}}{1+\Delta X/X} \times 100$$

Where ΔX = increase in flavor enhancer mass (g), X = flavor enhancer initial mass (g), and X_i = flavoring water content before exposure to environmental air (% g) ¹⁸.

Bulk and Tapped Density

The Bulk Density value is obtained by pouring an amount of powder flavor enhancer into a 10 mL measuring cup, adjusting it to 0 then weighing it. The sample weight obtained is then divided by the volume of the measuring cup (10 mL) so that the bulk density value is obtained. The same procedure is also used to obtain the tapped density value, except when the measuring cup which has been filled with the sample is tapped mechanically until it reaches a constant volume. Tapped density is calculated using the same formula as bulk density ^{19,20}.



Compressibility Index and Hausner Ratio

Compressibility index or Carr index and Hausner ratio were used to measuring the flow power of powder samples. Both are obtained from the density of the mass and tapped density of the flavor enhancer using the following equation ²¹.:

$$\text{Carr index (\%)} = \frac{\text{bulk density} - \text{tapped density}}{\text{tapped density}} \times 100$$

$$\text{Hausner ratio} = \frac{\text{tapped density}}{\text{bulk density}}$$

Wettability

Wettability was acquired after some flavor enhancer samples (10 g) were poured into 100 mL of distilled water that was already available in a 250 mL chemical glass. The time it takes for the sample to first touch the water surface until it is completely wet is a wettability value ²².

Water Solubility Index (WSI) and Water Absorption Index (WAI)

The water solubility index (WSI) was obtained by careful weighing of the flavor-enhancing powder 1.0 g, mixed in 30 mL of water, and incubated for 30 minutes in a water bath (Memmert WNB 10) at 30 °C. The mixture was then centrifuged (Gemmy PLC-03 8 Hole) for 15 minutes at 3000 rpm. The supernatant obtained was collected into a known weight of petri dishes, while the residue was weighed after drying for 8 hours in an oven (Binder ED 53) at 105 °C and expressed as the WSI value that had been accumulated with the initial sample weight (1.0 g). The water absorption index (WAI) is calculated based on the mass of solids remaining in the supernatant divided by the initial sample weight (1.0 g) ²³.



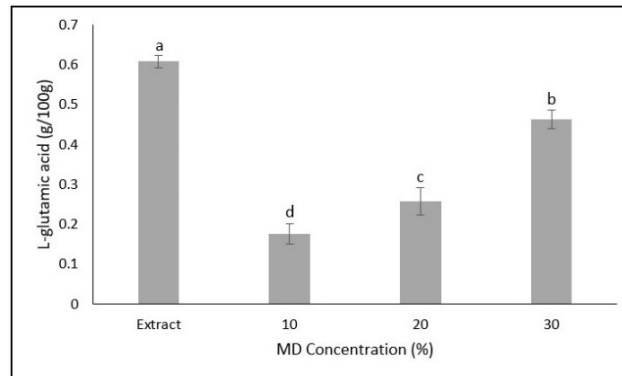
Morphology Characterization and Particle Size Measurement

Morphology characterization of the flavor enhancing powder was analyzed using an analytical scanning electron microscope (JSM-6510 LA, Jeol Ltd.). Particle size distribution was measured using a particle size analyzer LLPA-C10 (Labtron Equipment Ltd.), using the principle of laser light scattering, with a measurement range for dry disperse 0.01 - 2000 μm .

Results and Discussion

Glutamic Acid Content

The presence of glutamic acid in flavor enhancers is the most significant factor since it influences the taste of umami generated. L-glutamic acid is 0.61 g/100 g in Sargassum aquifolium extract. MD as a coating material is quite effective in protecting umami compounds from Sargassum aquifolium extract, where microcapsules with a 30 % MD concentration have the L-glutamic acid 0.46 g/100 g, while the lowest is at 10 % MD concentration (0.18 g/100 g). This indicates that MD has a chemical structure suitable for the core material, strengthened by previous research¹⁶. The chemical structure of the wall material that is not suitable will cause the coating of the core material to be not optimal so that a lot of it is wasted. The smaller the particle size, the more likely it will form a whole spherical structure like a ball which is known to be able to maintain the flavor-enhancing compounds optimally²⁴. MD is also known to be able to significantly increase the thermal stability of flavor enhancing microcapsules and improve the controlled release of microcapsules for up to 60 minutes in boiling water^{12,13}.



Diiferent letter (a, b, c) indicated significant ($p < 0.05$) different

Figure 1. L-Glutamic Acid Content of Umami Flavor Enhancing Microcapsules

Moisture Content and a_w

The umami flavor enhancer from seaweed has low moisture content and a_w (Table 1), indicating good efficiency of the drying process and product stability. Microbial growth will not be optimal, so the product shelf life will be long²⁰. This result follows other studies, which used MD as a coating material in the encapsulation process for umami compounds⁸, while Fazaili *et al.*,²⁵ also observed a decrease in water content with an increase in the concentration of the carrier material which is dried with various concentrations of MD. The use of MD in the flavor-enhancing microencapsulation process resulted in moisture content within the desired range (3.10 - 3.63%). The water content of microcapsules coated with MD by spray drying generally ranges from 2.11 to 4.66%^{26,27}.

Similar to water content, the a_w value of the flavor enhancer also decreases with the addition of MD as a coating material, in line with research conducted by Nambiar *et al.*,²⁸. However, excessive concentrations of MD will cause the product to stick to the nozzle and block the hot steam. The increase in MD up to 30% caused the a_w value of the product to decrease from 0.25 to 0.23, which was previously confirmed by Cao *et al.*,²⁹. a_w values below 0.60 for powder products are good, able to suppress microbial growth, while a_w values of 0.2 - 0.4 are considered the most optimal



because they are stable against adverse reactions such as oxidation, browning, hydrolytic, and enzymatic^{30,31}.

Tabel 1. Water content, a_w , hygroscopicity, water soluble index, and water absorption index of microcapsules

Concentration of MD	Water Content (%)	a_w	Hygroscopicity (%)	WSI (%)	WAI (%)
10%	3.63 ± 0.11^c	0.26 ± 0.02^c	20.56 ± 0.61^c	93.18 ± 0.43^a	0.03 ± 0.01^a
20%	3.23 ± 0.05^b	0.23 ± 0.01^b	17.88 ± 0.38^b	93.46 ± 0.50^a	0.05 ± 0.01^a
30%	3.10 ± 0.03^a	0.21 ± 0.01^a	15.47 ± 0.42^a	94.49 ± 0.18^a	0.06 ± 0.01^a

Note: The data are representations of the mean values \pm standard deviation. Different superscripts in the same column showed statistically significant differences ($p < 0.05$).

Hygroscopicity

Hygroscopicity in the food sector is closely related to the porosity and amorphous sugar content of the product. The powder produced by spray-drying tends to form amorphous solids. The process of evaporation of water material takes place quickly so that the product is more hygroscopic³².

The umami flavor enhancer has a fairly good hygroscopicity value with a value range of 15.47 - 20.56%, higher than that reported by Gagneten *et al.*,³³. Apart from being hygroscopic, spray dried products have a porous surface structure and a low glass transition temperature (Tg). Improper handling after drying, allows the product moisture content to increase. The addition of coatings is very effective in correcting these deficiencies^{24,34}. MD has anti-hygroscopic properties which can change the balance of hydrophilic/hydrophobic particles, which results in lower water absorption¹⁵.

Water Solubility Index and Water Absorption Index

The ideal powder product has a high WSI value. There can be no significant differences in the sample WSI. However, the powder WSI value was higher when the MD concentration increased. In



general, the solubility of the product was very good (93.18 - 94.49%). The presence of MD increased the solubility of atomized samples. This is due to the very high hydroxyl (OH) group in the MD molecule. MD also produces a more porous powder microstructure, so that the powder will more easily dissolve in water ^{18,35}. The umami compounds in the extract are also hydrophilic. Umami compounds will interact with taste receptors when they meet saliva, one of the unique and important characteristics of food flavor enhancers ⁸.

Unlike the case with WSI, WAI is a solid that remains after the centrifugation process. The concentration of WAI is generally very small and was confirmed in this study. Taste enhancers had WAI values in the range of 0.03 - 0.06%. There was no statistically significant difference. The same result was also reported by Vidović *et al.*, ²³, the low value of WAI was influenced by the hydrophilic group of the particles that bind water molecules which then form a gel. The values of WSI and WAI are the determining factors for the quality of powders used in the food industry. The industry prefers powder products with high WSI values and low WAI. Powders with poor solubility can cause high economic losses for companies ³⁶.

Wettability, Particle Size, and Morphological Characteristics of Microcapsules

Apart from high solubility, flavor enhancers should ideally also have a fast wettability, do not float, and sink completely. The average wettability time of the seaweed flavor enhancer ranged from 427 to 689 s, faster than the wettability of the sumac extract microcapsules (1239 - 3263 s) reported by Caliskan & Dirim ³⁰, but longer than the wettability of the spray-dried blackberry microcapsules with the same coating material ³⁷. Although it has high solubility and porous particle structure ^{38,39}, the main component of MD preparation is starch so it requires a longer wettability time ⁴⁰. There are several ways to speed up the wettability time, such as the addition of inulin in



the coating material formulation which has been confirmed to be able to significantly shorten the wettability time of the spray drying powder³⁶. Several other aspects such as a decrease in the drying temperature (inlet or outlet) and the concentration of the coating material will cause a faster wettability time, due to the size and structure of the resulting particles.

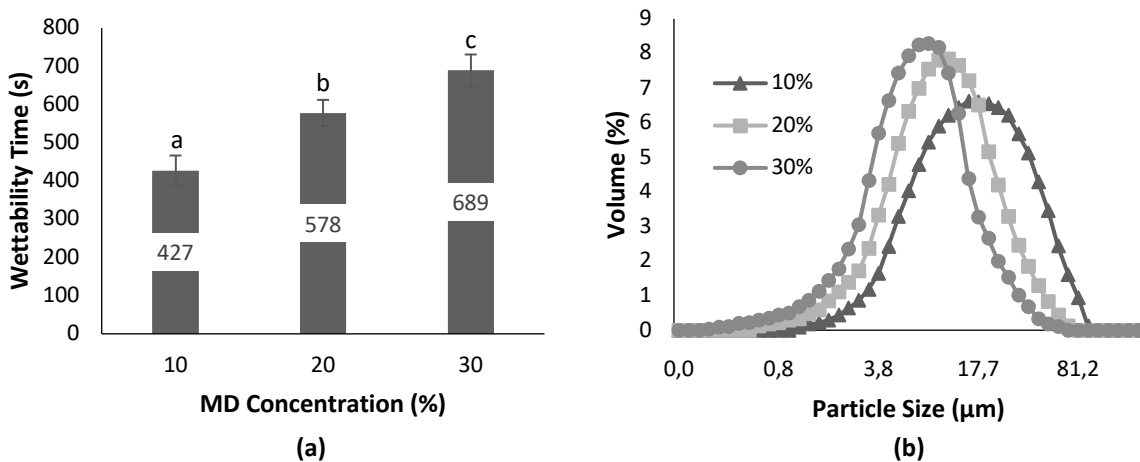


Figure 2: (a) Wettability time, and (b) Microcapsule Particle Size Distribution

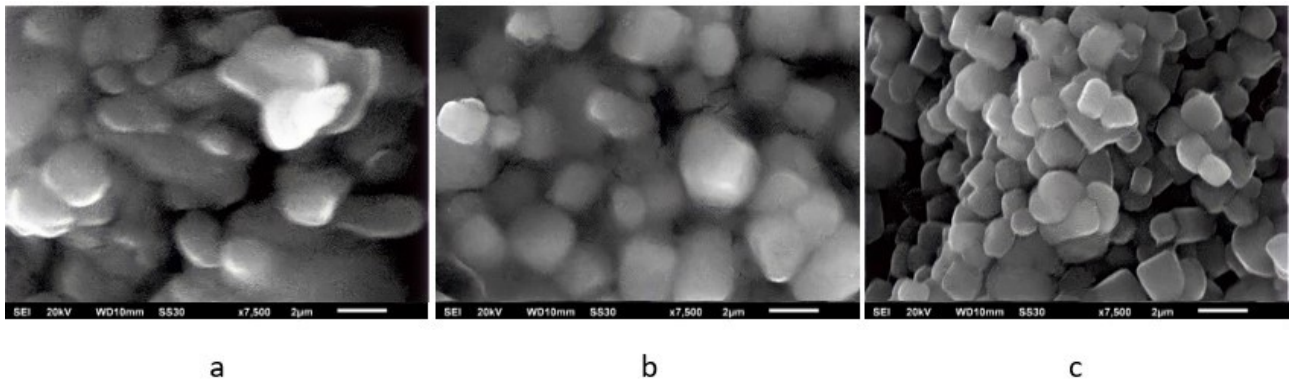


Figure 3: Morphology of umami flavor enhancer with various concentrations of MD (a) 10 %, (b) 20 %, and (c)30 %

The particle size of the umami flavor enhancers of *Sargassum aquifolium* ranges from 0.19 - 94.57 µm, smaller than that reported by Mayasari *et al.*,¹⁶ (43.14 - 101.71 µm). The particle size distribution of each coating concentration was observed, flavor enhancers with MD 30% produced the smallest particle size distribution (0.19 – 59.371 µm) with a dominant size of 5.21 - 11.17 µm



(47.51 %), and a peak size of 8.23 μm , flavor enhancers with MD 20% produced particles with a size distribution of 0.62 - 69.60 μm , dominant size 8.23 - 7.21 (38.06 %, with a peak size of 11.17 μm , while flavor enhancers with 10% MD had the largest particle size distribution (1.13 - 94.57 μm) with the size dominant 11.17 - 27.90 μm (45.05%), and peak particle size at 15.16 μm .

Sargassum aquifolium contains alginate polysaccharides. These hydrocolloid compounds cause less perfect encapsulation, irregular particle shape, and stick together. This condition can be seen in Figure 3a. An increase in MD of up to 30 % results in a smoother microcapsule surface and a more uniform and even shape of the particles (Figure 3c). Medina-Torres *et al.*,⁴¹ reported that the results of microcapsules by spray drying with MD coating material have a very small size distribution (10 - 40 μm), with a rough, hollow, irregular surface morphology with structural cracks on the surface. The high drying temperature will result in smaller particles with finer and more rounded morphology^{16,35}.

Colour Parameters

The color attribute is one of the sensory attractions that need attention. Ideally, the flavor enhancer should be a bright color so that it doesn't affect the final color of the product when added. The seaweed extract used tends to be brown with details $L^* = 58.31$; $a^* = 6.29$ and $b^* = 20.16$, while the MD used is bright white ($L^* = 97.83$; $a^* = 0.21$ and $b^* = 1.94$). The L^* value of flavor enhancement significantly increased (76.76 to 81.49), resulting from the dominant white color of MD⁴². a^* (4.32 to 3.16) and b^* (16.35 to 14.29) values decreased as the coating agent concentration increased. MD produced good retention of flavor-enhancing pigments. This result was in line with the color change of the tea water extract microcapsules coated MD with spray drying reported by Nadeem *et al.*⁴³.



Table 2. CIELAB colour parameters of microcapsules

Concentration of MD	L^*	a^*	b^*	C°	Hue Angle
10%	76.76 ± 0.91^a	4.32 ± 0.12^c	16.35 ± 0.22^c	16.91 ± 0.23^c	75.18 ± 0.37^a
20%	79.60 ± 0.97^b	3.46 ± 0.09^b	15.42 ± 0.15^b	15.80 ± 0.16^b	77.35 ± 0.24^b
30%	81.49 ± 0.21^c	3.16 ± 0.33^a	14.29 ± 0.56^a	14.64 ± 0.56^a	77.52 ± 1.33^c

Note: The data are representations of the mean values \pm standard deviation. Different superscripts in the same column showed statistically significant differences ($p < 0.05$).

The hue angle is related to the color produced, the value 0° representing red and 90° representing yellow. With increasing MD concentration, the color change towards yellow is getting bigger, where the hue angle from 75.18 to 77.52, while the chroma value decreases (16.91 to 14.64), it is possible because high temperatures cause the color pigment to degrade slightly²⁸. Caparino *et al.*,¹⁸ also explained that spray drying resulted in very small particle size so that the resulting mango powder was brighter. The increase in brightness will cause a decrease in color sharpness (Chroma) in addition to the effect of white MD.

Bulk and Tapped Density, Carr Index and Hausner Ratio

Powder flowability can be determined by the value of bulk and tapped density, Carr index, and Hausner ratio. The bulk and tapped density values for the umami flavor enhancer can be seen in Table 3. The bulk density of seaweed flavor enhancer powder was found to be greater in microcapsules coated with 30 % MD (0.46 g/mL), as well as the tapped density of powder at the same concentration (0.54 g/mL). MD particles that are bigger than the core particles will cause the density of the powder produced to increase with the addition of MD. Besides, powders with lower water content are also known to have a greater density^{43,44}. This is in line with what Singh *et al.*,⁴⁵ reported, an increase in the concentration of MD up to 300 % which was dried by spray drying would cause the tapped density of powder to increase from 0.38 - 0.44 g/mL.



The increase in coating material concentration also has an impact on decreasing the volume of particles, which is caused by decreased air formation in the structure, so that the bulk and tapped density increases¹⁹. In contrast to coating materials, an increase in intake air temperature tends to result in a lower bulk particle density¹⁶. An increase in inlet temperature followed by a decrease in the feed flow rate causes the outer dry layer of the droplet surface to form rapidly, the outside will form a moisture-proof film while the inside forms a hollow structure²⁰. When the hollow structure decreases, the particle volume decreases, which affects the cohesiveness of the particles. The cohesiveness of the structure is an important indicator of powder flow properties, expressed by Carr index, and Hausner ratio values.

Table 3. Bulk and tapped density, Carr index, and Hausner ratio of microcapsules

Concentration of MD	Bulk Density (g/mL)	Tapped Density (g/mL)	Carr Index (%)	Hausner Ratio
10 %	0.31 ± 0.02 ^a	0.38 ± 0.03 ^a	18.60 ± 0.93 ^c	1.23 ± 0.01 ^c
20 %	0.37 ± 0.02 ^b	0.45 ± 0.02 ^b	17.41 ± 0.60 ^b	1.21 ± 0.01 ^b
30 %	0.46 ± 0.02 ^c	0.54 ± 0.03 ^c	14.17 ± 0.45 ^a	1.17 ± 0.01 ^a

Note: The data are representations of the mean values ± standard deviation. Different superscripts in the same column showed statistically significant differences ($p < 0.05$).

Deshmukh *et al.*,⁴⁶ stated that spray drying generally results in a narrower particle size distribution with excellent flow properties. High Carr index, and Hausner ratio values indicate higher particle cohesiveness, and poor flowability²⁰. According to Lebrun *et al.*,²¹ a good powder has the criteria for the Carr index value of ≤ 15 and the Hausner Ratio value of ≤ 1.18 . The flowability of the flavor enhancing powder with MD 10% and 20% was still acceptable, the best flowability was produced after the addition of 30% coating material with Carr index values of 14.17 (good) and Hausner ratio 1.17 (good). These results are consistent with the findings reported by Cao *et al.*,²⁹. Products with higher Hausner ratio tend to be cohesive, characterized by a higher moisture content⁴⁰. Also,



particle size, hardness, surface shape, elasticity to interstitial air determine the cohesiveness of the powder which determines the product flowability¹⁵.

Conclusion

Based on the analysis of physical and chemical characteristics, the best umami flavor enhancing microcapsules from the *Sargassum aquifolium* seaweed extract from spray drying were produced by adding 30% MD. L-glutamic acid levels in the umami flavor enhancing microcapsules reach 0.46 g/100 g. Microcapsules have low moisture content (3.10 %), a_w (0.21), and Hg (15.47 %), which are good for product shelf life because they are able to withstand the rate of damage both biologically, chemically, and physically. Although the product wettability time is relatively long (689 s), the microcapsules have excellent solubility (WSI 94.49 % and WAI 0.06 %) and are favored by the industrial world. The powder is slightly yellowish-brown in color with good brightness (L^* 81.49, a^* 3.16, b^* 14.29, C° 14.64, H° 77.52). The product flowability and cohesiveness were good, as indicated by the bulk and tapped density values of 0.46 g/mL and 0.54 g/mL, then Carr index 14.17 and Hausner ratio 1.17. The powder particle size ranged from 0.19 to 59.37 μm with smooth surface morphology and uniform shape.

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Conflict of Interest

The authors declare no conflict of interest.



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